

In Session Practice Problems – Thermodynamics (EGN 3343)

January 2024

Hello everyone,

These are some problems that, in my experience, provide students with a wider understanding of the topics covered in Chapter 4 of the book. I will go over these and other problems during my sessions. I highly recommend that you attend these sessions to solve any doubts.

Disclaimer: There is no guarantee that any of these problems will be included in any exam, so the best way to approach these problems is like practice problems that will help you familiarize yourself with important concepts learned during the semester. Finally, do not use this guide as your ONLY study resource for the exams.

Important Note: All problems and diagrams presented here were extracted from Cengel, Yunus, et al. Thermodynamics: An Engineering Approach. Available from: Yuzu Reader, (9th Edition). McGraw-Hill Higher Education (US), 2018.

4-18E During an expansion process, the pressure of a gas changes from 15 to 100 psia according to the relation $P = a + b$, where $a = 5 \frac{\text{psia}}{\text{ft}^3}$ and b is a constant. If the initial volume of the gas is 7 ft^3 , calculate the work done during the process. Answer: 181 Btu

4.18E

$$P_0 = 15 \text{ psi} \quad P_P = 100 \text{ psi}$$

$$a = 5 \text{ psi/ft}^3 \quad b = \text{constant}$$

$$P = aV + b$$

We go back to the work formula

$$W = \int P dV ?$$

$$W = \int_{V_0}^{V_f} aV + b dV$$

We need the final volume, so we go back to the equation of pressure given

$$P = aV + b \quad ?$$

Besides V_f we have a second unknown b , but since we have our initial conditions, we could solve for b

$$b = P - aV = 15 \text{ psi} - 5 \frac{\text{psi}}{\text{ft}^3} (7 \text{ ft}^3)$$

$$b = -20 \text{ psi}$$

Now that we have b
we can solve for our final
volume

$$p = aV + b \rightarrow \frac{p-b}{a} = V$$

$$V = \frac{100 \text{ psi} - (-20 \text{ psi})}{5 \frac{\text{psi}}{\text{ft}^3}} = \underline{24 \text{ ft}^3}$$

We can go back and
solve our integral

$$W = \int_7^{24} 5V - 20 \, dV$$

$$W = \left. \frac{5}{2} V^2 - 20V \right|_7^{24}$$

$$W = \frac{5}{2} (24^2 - 7^2) - 20(24 - 7)$$

$$W = 977.5 \text{ psi} \cdot \text{ft}^3$$

But the problem require
Btu not $\text{psi} \cdot \text{ft}^3$, so

$$W = 977.5 \text{ psi} \cdot \text{ft}^3 \left(\frac{1 \text{ Btu}}{5.404 \text{ psi} \cdot \text{ft}^3} \right)$$

$$W = 180.884 \text{ Btu}$$

$$\approx \underline{181 \text{ Btu}}$$

4-19 A piston-cylinder device initially contains 0.4 kg of nitrogen gas at 160 kPa and 140°C. The nitrogen is now expanded isothermally to a pressure of 100 kPa. Determine the boundary work done during this process. Answer: 23.0 kJ

4-19. $P_0 = 160 \text{ kPa}$ $T = 140^\circ\text{C}$
 $m = 0.4 \text{ kg}$ $P_F = 100 \text{ kPa}$

$$\int P dV$$

$$PV = RTm$$

$$V = \frac{RTm}{P}$$

$$V = RTm P^{-1}$$

$$\frac{dV}{dP} = -\frac{RTm}{P^2}$$

$$W = -\int \frac{RTm}{P} dP$$

$$W = -RTm \int_{P_0}^{P_F} \frac{1}{P} dP$$

$$W = -RTm \ln(P)$$

$$W = -RTm (\ln(100) - \ln(160))$$

$$W = RTm (\ln(160) - \ln(100))$$

$$W = 0.297 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} (140 + 273.15 \text{ K}) (0.4 \text{ kg})$$

$$(\ln(160) - \ln(100))$$

$$W = 22.29 \text{ kJ}$$

4-19 (Second approach)

$$m = 0.4 \text{ kg} \quad P_0 = 160 \text{ kPa} \quad T = 140^\circ \text{C}$$

$$P_F = 100 \text{ kPa}$$

$$W = P_1 V_1 \ln \frac{V_2}{V_1} \quad \text{equation 4.7}$$

We need to find V_1 and V_2 , so we will use the ideal gas equation

$$PV = RTm \rightarrow V = \frac{RTm}{P}$$

$$V_1 = \frac{0.287 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} (140 + 273.15 \text{ K}) (0.4 \text{ kg})}{160 \text{ kPa}}$$

$$V_1 = 0.296435 \text{ m}^3$$

$$V_2 = \frac{0.287 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} (140 + 273.15 \text{ K}) (0.4 \text{ kg})}{100 \text{ kPa}}$$

$$V_2 = 0.474296 \text{ m}^3$$

Now we can plug in in our work equation

$$W = 160 (0.296435) \ln \left(\frac{0.474296}{0.296435} \right)$$

$$W = 22.29 \text{ kJ}$$

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4-34E A rigid 1 ft³ vessel contains R-134a originally at -20°F and 27.7 percent quality. The refrigerant is then heated until its temperature is 100°F. Calculate the heat transfer required to do this. Answer: 84.7 Btu

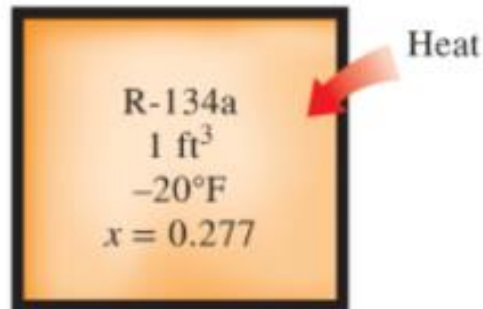


FIGURE P4-34E

4-34E R-134A
 $V = 1 \text{ ft}^3$ $T_0 = -20^\circ \text{F}$ $x = 27.7$ $T_F = 100^\circ \text{F}$

$$\Delta E = E_{\text{in}} - E_{\text{out}}$$

$$[U_2 + \cancel{\frac{1}{2} m v_2^2} + \cancel{m g h_2} + \cancel{\rho V_2}] - [U_1 + \cancel{\frac{1}{2} m v_1^2} + \cancel{m g h_1} + \cancel{\rho V_1}] = [Q_{\text{in}} + \cancel{W_{\text{in}}}] - [Q_{\text{out}} - \cancel{W_{\text{out}}}]$$

$$Q_{\text{in}} = U_2 - U_1$$

$$Q_{\text{in}} = m(u_2 - u_1)$$

First we need to find mass, we can use the specific volume and table A11E

$$v = \frac{V}{m} \rightarrow m = \frac{V}{v}$$

$$v = v_f + x v_{fg}$$

$$v = 0.01156 + 0.277(3.4424 - 0.01156)$$

$$v = 0.961902 \text{ ft}^3/\text{lbm}$$

$$m = \frac{1 \text{ ft}^3}{0.961902 \text{ ft}^3/\text{lbm}} = 1.03960 \text{ lbm}$$

Now we can also find u_1 in a similar way we found v

$$u = u_f + x u_{fg}$$

$$u = 6.014 + 0.277(85.887)$$

$$u = 29.8046 \frac{\text{Btu}}{\text{lbm}}$$

Now in the same table we can go to $T = 100^\circ\text{F}$ in an effort to find u_2 , but since our V and m remain constant, our v must also remain constant. If we compare v with v_f and v_g , we notice that our substance is superheated, so we need to go to table A-13E. We notice that our v at 100°F is between $P = 50 \text{ psia}$ and $P = 60 \text{ psia}$ which means our u_2 is between $111.56 \frac{\text{Btu}}{\text{lbm}}$ and $111.17 \frac{\text{Btu}}{\text{lbm}}$, so we need to interpolate:

$$\frac{u_2 - 111.17}{0.961902 - 0.9072} = \frac{111.56 - 111.17}{1.1043 - 0.9072}$$

$$u_2 = 111.278 \frac{\text{Btu}}{\text{lbm}}$$

Now we can plug back in our energy equation

$$Q_{in} = 1.03960 (111.278 - 29.8046)$$
$$Q_{in} = 84.7003 \approx \underline{84.7 \text{ Btu}}$$

4-72 A mass of 15 kg of air in a piston–cylinder device is heated from 25 to 95°C by passing current through a resistance heater inside the cylinder. The pressure inside the cylinder is held constant at 300 kPa during the process, and a heat loss of 60 kJ occurs. Determine the electric energy supplied, in kWh. Answer: 0.310 kWh

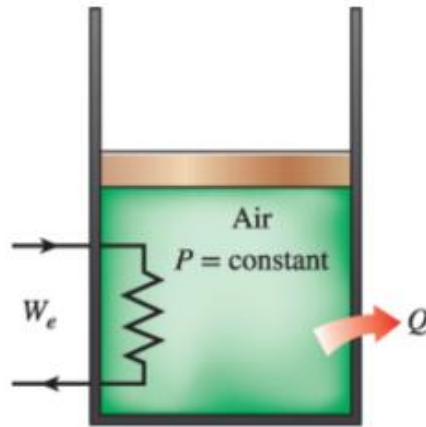


FIGURE P4-72

4-72
 $m = 15 \text{ kg}$ $T_0 = 25^\circ\text{C}$ $T_f = 95^\circ\text{C}$
 $P = 300 \text{ kPa}$ $Q = -60 \text{ kJ}$

The first step would be to set up the energy equation and introduce some important values

$$\Delta E = E_{in} - E_{out}$$

$$[U_2 + \cancel{\frac{1}{2}mV_2^2} + \cancel{mgh_2}] - [U_1 + \cancel{\frac{1}{2}mV_1^2} + \cancel{mgh_1}] = [Q_{in} + W_{in}] - [Q_{out} + W_{out}]$$

We don't have potential nor kinetic energy

We don't have heat in

heat lost

Work done by resistor

Work done by piston

$$U_2 - U_1 = W_{in} - Q_{out} - W_{out}$$

We isolate work in since that's the value we need

$$W_{in} = [U_2 - U_1] + Q_{out} + W_{out}$$

$$W_{in} = m [U_2 - U_1] + Q_{out} + W_{out}$$

We can replace these values with $\Delta u = C_v(T_2 - T_1)$

since P is constant

$$W = \int P dv$$

$$W = PC(V_2 - V_1)$$

From Table A-2 $C_v = 0.718$

$$W_{in} = mC_v(T_2 - T_1) + Q_{out} + P(V_2 - V_1)$$

$$W_{in} = 15(0.718)(95 + 273 - (25 + 273)) + 60 \text{ kJ} + 300(5.28295 - 4.27845)$$

$$W_{in} = 1115.25 \text{ kJ}$$

$PV = RTm$
 $V = RTm/P$
 $V_1 = 0.287(25 + 273)(15)/300$
 $V_1 = 4.27845 \text{ m}^3$
 $V_2 = 0.287(95 + 273)(15)/300$
 $V_2 = 5.28295 \text{ m}^3$

Now we just have to convert to kWh

$$1115.52 \text{ kJ} \left(\frac{1 \text{ kWh}}{3600 \text{ kJ}} \right) = 0.309797 \text{ kWh}$$
$$\approx 0.310 \text{ kWh}$$

\rightarrow (1h) $1 \text{ kW} = \frac{1 \text{ kJ}}{\text{s}} (1 \text{ h})$
 $1 \text{ kWh} = 1 \text{ kJ} (3600 \text{ s})$
 $1 \text{ kWh} = 3600 \text{ kJ}$
 $1 \text{ h} = 3600 \text{ s}$